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# CBCS SCHEME

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18ME33

## Third Semester B.E. Degree Examination, Jan./Feb. 2021 **Basic Thermodynamics**

Time: 3 hrs.

Max. Marks: 100

**Note:** 1. Answer any **FIVE** full questions, choosing **ONE** full question from each module.  
2. Use of thermodynamic data handbook is permitted.

### Module-1

- 1 a. Explain microscopic and macroscopic approaches to thermodynamics. (06 Marks)  
b. State and explain Zeroth law of thermodynamics. What is diathermal and adiabatic wall? (06 Marks)  
c. The temperature  $t$  on a Celsius thermometer scale is defined in terms of property  $P$  by the relation  $P = e^{\frac{(t-B)}{A}}$  where  $A$  and  $B$  are constants. At ice point and steam points the value of  $P$  is 1.86 and 6.81 respectively. Find the value of ' $t$ ' for  $P = 2.5$ . (08 Marks)

OR

- 2 a. With examples distinguish between:  
(i) Intensive and extensive property  
(ii) Point and path function  
(iii) Thermodynamic equilibrium (10 Marks)  
b. In 1709m Newton proposed a linear temperature scale where ice point and normal human body temperature are maintained as two fixed points of  $0^\circ N$  ad  $12^\circ N$  respectively. The temperature of human body on the Celsius scale is  $36^\circ C$ . Obtain relation between Newton scale and Celsius scale. (10 Marks)

### Module-2

- 3 a. Obtain the expression for displacement adiabatic work. (06 Marks)  
b. Define heat and work with reference to thermodynamic point of view and also the sign convention of heat and work. (06 Marks)  
c. A cylinder contains 1 kg of certain fluid at an initial pressure of 20 bar. The fluid is allowed to expand reversibly behind a piston according to law  $PV^2 = \text{constant}$  until the volume is doubled. The fluid is then cooled reversibly at constant pressure until the piston regains its original position. Heat is then supplied reversibly with the piston firmly locked in position until the pressure rises to its original value of 20 bar. Calculate the net work done by the fluid for an initial volume of  $0.05 \text{ m}^3$ . (08 Marks)

OR

- 4 a. Apply steady flow energy equation to each of the following:  
(i) Boiler (ii) Nozzle (iii) Centrifugal pump  
(iv) Throttling device (v) Turbine (10 Marks)  
b. The working fluid in a steady flow process flows at the rate of 220 kg/min. the fluid rejects 100 kJ/s of heat passing through the system. The fluid enters at a velocity of 320 m/s, pressure of 6 bar, internal energy 2000 kJ/kg, specific volume of  $0.36 \text{ m}^3/\text{kg}$  and leaves the system at a velocity of 140 m/s, pressure of 1.2 bar, internal energy 1400 kJ/kg, specific volume of  $1.3 \text{ m}^3/\text{kg}$ . Determine the power output in MW. The change in potential energy is neglected. (10 Marks)

**Module-3**

- 5 a. Prove that Kelvin-Planck statement and clausius statements of second law of thermodynamic are equivalent. **(10 Marks)**
- b. A reversible heat engine operates between two reservoirs at temperature of  $600^{\circ}\text{C}$  and  $40^{\circ}\text{C}$ . The engine drives a reversible refrigerator which operates between reservoirs at temperature of  $40^{\circ}\text{C}$  and  $-20^{\circ}\text{C}$ . The heat transfer to the heat engine is 2000 kJ and net work output of combined engine refrigerator plant is 360 kJ. Evaluate the heat transfer to the refrigerant and net heat transfer to the reservoir at  $40^{\circ}\text{C}$ . **(10 Marks)**

**OR**

- 6 a. Show that entropy is a property of the system. **(04 Marks)**
- b. Derive the maximum work attainable from a finite body and a thermal energy reservoir. **(10 Marks)**
- c. A lump of steel of mass 10 kg at  $627^{\circ}\text{C}$  is dropped in 100 kg of oil at  $30^{\circ}\text{C}$ . The specific heats of steel and oil are 0.5 kJ/kgK and 3.5 kJ/kgK respectively. Calculate the entropy change of steel, the oil and the universe. **(06 Marks)**

**Module-4**

- 7 a. Explain the concept of available and unavailable energy. **(04 Marks)**
- b. Write Maxell relations and explain the terms involved. **(06 Marks)**
- c. A vessel of volume  $0.04 \text{ m}^3$  contains a mixture of saturated water and saturated steam of a temperature of  $250^{\circ}\text{C}$ . The mass of liquid present is 9 kg. Find the pressure, mass, specific volume, enthalpy and internal energy. **(10 Marks)**

**OR**

- 8 a. With a neat sketch, explain the working of combined separating and throttling calorimeter. **(10 Marks)**
- b. Steam at 10 bar and dry state is cooled under constant pressure until it becomes 0.85 dry. Using steam tables, find the work done, change in enthalpy, heat transferred and change in entropy. **(10 Marks)**

**Module-5**

- 9 a. Determine the Vander Waal's constant in terms of critical properties. **(08 Marks)**
- b. Explain the following:
- (i) Generalized compressibility chart
  - (ii) Law of corresponding state
  - (iii) Compressibility factor **(04 Marks)**
- c. Determine the pressure exerted by carbon dioxide in a container of  $1.5 \text{ m}^3$  capacity when it contains 5 kg at  $27^{\circ}\text{C}$  using (i) Ideal gas equation (ii) Vander Waal's equation. Take Vander Waal's constant for  $\text{CO}_2$  as  $a = 364.3 \text{ kNm}^4/\text{kgmol}^2$ ,  $b = 0.0427 \text{ m}^3/\text{kgmol}$ . **(08 Marks)**

**OR**

- 10 a. Explain Dalton's law if partial pressure and Amagat's law of additive volumes with reference to ideal gas mixture. **(08 Marks)**
- b. Derive an expression for internal energy and enthalpy of gaseous mixtures. **(04 Marks)**
- c. A mixture of gases contains 1 kg of  $\text{CO}_2$  and 1.5 kg and  $\text{N}_2$ . The pressure and temperature of the mixture are 3.5 bar and  $27^{\circ}\text{C}$ . Determine for the mixture :
- (i) The mass and mole fraction of each constituent gas
  - (ii) Average molecular weight
  - (iii) The partial pressure **(08 Marks)**

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**[SPAM] Re: Sir, Regarding Discrepancy in the question paper(18ME33)**

"virupaxi bagodi" <virupaxibagodi@yahoo.com>  
To: boe@vtu.ac.in

March 26, 2021 11:50 AM

Dear Sir,

The corrections are correct and approved.

Thanking you with warm regards.

Sincerely,  
Dr. Virupaxi Bagodi  
Principal  
Government Engineering College,  
TALAKAL - 583238, India  
E-mail: [virupaxibagodi@yahoo.com](mailto:virupaxibagodi@yahoo.com)  
Cell: +91 94 49 973293

On Friday, 26 March, 2021, 11:38:47 am IST, <[boe@vtu.ac.in](mailto:boe@vtu.ac.in)> wrote:

**"APPROVED"**  
*Rang SE*  
Registrar (Evaluation)  
Visvesvaraya Technological University  
Bengaluru - 590018

## Basic Thermodynamics - 18ME33.

Q9.C → To determine the pressure exerted by  $O_2$  using (i) Ideal gas eq<sup>n</sup> (ii) van der waal's eq<sup>n</sup>

The solution shows that by

(i) Ideal gas eq<sup>n</sup>  $P = \frac{mRT}{V}$

$$P = 1.889 \text{ bar or } 188.9 \text{ kPa}$$

(ii) van der waal's eq<sup>n</sup>

$$P = 3.6 \text{ bar} - \text{which is incorrect.}$$

The correct answer is :

$$P = \underline{1.870 \text{ bar or } 187.0 \text{ kPa}}$$

$$P = \frac{RT}{V-b} - \frac{a}{V^2}$$

Kindly correct the scheme & solution.

Dr. K. M. AKKoh ~~missed~~  
Dr Ratan Pathil ~~missed~~  
Prof Manik R. ~~missed~~

Approved as suggested by  
charna BoE

"APPROVED"

Ram TE 26/03/2021  
Registrar (Evaluation)  
Visvesvaraya Technological University  
BELAGAVI - 590078

## [SPAM] Fw: Scheme and solutions

"virupaxi bagodi" <virupaxibagodi@yahoo.com>  
To: boe@vtu.ac.in, boe@vtu.ac.in

March 23, 2021 8:07 AM

Dear Sir,

Subject: Basic thermodynamics and Subject code: 18ME33, scheme and solutions are found correct.

Thanking you with warm regards.

Sincerely,  
Dr. Virupaxi Bagodi  
Principal  
Government Engineering College,  
TALAKAL - 583238, India  
E-mail: [virupaxibagodi@yahoo.com](mailto:virupaxibagodi@yahoo.com)  
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----- Forwarded message -----

**From:** Shanka naik <[shankarnaiksb@gmail.com](mailto:shankarnaiksb@gmail.com)>  
**To:** virupaxi bagodi <[virupaxibagodi@yahoo.com](mailto:virupaxibagodi@yahoo.com)>; Virupaxi Bagodi <[virupaxibagodi@gmail.com](mailto:virupaxibagodi@gmail.com)>  
**Sent:** Monday, 22 March, 2021, 10:08:38 pm IST  
**Subject:** Scheme and solutions

Respected sir:

Subject: **Basic thermodynamics** and Subject code: **18ME33**, scheme and solutions are found correct.

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Dr. Shankara Naik  
Department of Mechanical Engineering  
Government Engineering College  
Haveri-581110  
Karnataka

*"APPROVED"*  
*Ran* *eb E*  
Registrar (Evaluation)  
Fiveshaya Technological University  
BELAGAVI-590018



Scheme & Solution

Signature of Scrutinizer

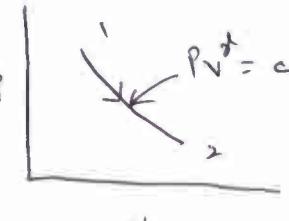
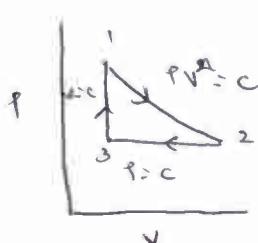
Subject Title : Basic Thermodynamics

Subject Code : 18ME33

Question Number	Solution	Marks Allocated
1a	<p>Microscopic Approach &amp; Macroscopic Approach</p> <p>It considers the behaviour of every molecule by using Statistical Methods. In Macroscopic approach we are concerned with the gross or average effects of many molecules in fractions. These effects can be measured such as pressure and temperature can be received by our sense. This approach greatly reduces the problem of complexity and this is known as classical thermodynamics.</p> <p>Large number of variables is needed to describe microscopic approach whereas only few properties are needed in macroscopic approach.</p> <p>The behaviour of system is found by using Statistical Method whereas analysis of Macroscopic system requires single Mathematical formulae.</p>	Ob Marks
b.	<p>Statement :-</p> <p>When a body A is in thermal equilibrium with body B and body B is in thermal equilibrium with body C then body A + c are in thermal equilibrium.</p>	

Question Number	Solution	Marks Allocated
	A diathermal wall is one that heat can pass through. It is made from a thermal conductor. It is essentially a thermal wall.	0 Marks
	An adiabatic wall is one that heat cannot pass through. It is made from a thermal insulator.	
C.	Given $P = e^{\frac{t-B}{A}}$ Taking ln on both sides $\ln P = \frac{t-B}{A} \Rightarrow t = A \ln P + B$	1 Mark
	$P_i = 1.82 \quad P_s = 6.81$ $t_i = A \ln P_i + B - \textcircled{1}$ $0 = A \ln 1.82 + B - \textcircled{2}$ $100 = A \ln 6.81 + B - \textcircled{3}$ $\textcircled{3} - \textcircled{2} \Rightarrow A = 77.04$ $B = -47.79$ Sub the value of A & B in eqn \textcircled{1}	1 Mark
	$t = A \ln P + B$ $t = 77.04 \ln 2.5 - 47.79$ $t = 22.80^\circ C$	2 Marks

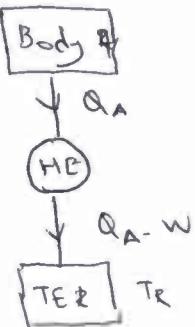
Question Number	Solution	Marks Allocated
2-a	<p>i) Intensive - Independent of Mass Ex: Pressure Extensive - Depend on the Mass Ex: Volume</p> <p>ii) Point function - Properties can be located as point in the coordinate axis Ex: Temperature lath function: Can't be located as point but can be represented as Area Ex: Work</p> <p>iii) Thermodynamic equilibrium states that when the pressure and temperature at all points are same and there is no velocity gradient then the system is said to be thermodynamic equilibrium</p>	10 Marks
b.	$t = ax + b \quad \text{--- (1)}$ $t_i = ax_i + b$ $t_s = ax_s + b$ $0 = ax_i + b \quad \text{--- (2)}$ $12 = ax_s + b \quad \text{--- (3)}$ $(3) - (2) \Rightarrow 12 = a(x_s - x_i)$ $a = \frac{12}{x_s - x_i}$ Sub a in eqn (2) $b = -12x_i$ Sub value of a & b in eqn (1) $t = \frac{12}{x_s - x_i} x - \frac{12x_i}{x_s - x_i}$ $t_i = 12 \frac{x - x_i}{x_s - x_i}$	01 Marks
	$t_c = ax + b \quad \text{--- (3a)}$ $t_i = 0 \quad t_s = 3b$ $0 = ax_i + b \quad \text{--- (4)}$ $3b = ax_s + b \quad \text{--- (5)}$ $(5) - (4) \Rightarrow 3b = a(x_s - x_i)$ $a = \frac{3b}{x_s - x_i}$ Sub a in eqn (4) $b = -\frac{3b}{x_s - x_i} x_i$ Sub value of a & b in eqn (3a) $t = \frac{3b}{x_s - x_i} x - \frac{3bx_i}{x_s - x_i}$ $t_i \geq 3b \frac{x - x_i}{x_s - x_i}$	02 Marks
		02 Marks

Question Number	Solution	Marks Allocated
	$\frac{t_{in}}{12} = \frac{t_c}{36}$ $3t_{in} = t_c$	03 Marks
3a	$W = \int P dV$ Adiabatic $PV^\gamma = c$ $P = \frac{c}{V^{\gamma}}$ $W = \int_{V_1}^{V_2} \frac{c}{V^{\gamma}} dV \Rightarrow \frac{c}{\gamma-1} \left[ V^{-\gamma+1} \right]_{V_1}^{V_2} \Rightarrow \frac{P_2 V_2^{\gamma} - P_1 V_1^{\gamma}}{\gamma-1}$  $\Rightarrow \frac{P_2 V_2 - P_1 V_1}{\gamma-1} = \frac{P_1 V_1 - P_2 V_2}{\gamma-1}$	06 Marks
b	Work - Solar effect could be reduced by using <sup>up</sup> of weight external to the surroundings Heat : Measure of degree of coldness (or) hotness	06 Marks
		
c	Given $m = 1 \text{ kg}$ , $T_1 = 20 \text{ bar}$ , $V_1 = 0.05 \text{ m}^3$ $V_2 = 2V_1 = 0.1 \text{ m}^3$	 02 Marks

Question Number	Solution	Marks Allocated
	<p>Process 1-2 Polytropic</p> $P_1 V_1^{\frac{1}{n}} = P_2 V_2^n$ $P_2 = P_1 \left( \frac{V_1}{V_2} \right)^{\frac{1}{n}} = 20 \left[ \frac{1}{2} \right]^2 = 5 \text{ bar}$ $W.D = \frac{P_1 V_1 - P_2 V_2}{n-1} = \frac{(20 \times 10^2 \times 0.05) - (5 \times 10^2 \times 0.1)}{2-1}$ $W.D = 50 \text{ KJ}$	
	<p>2-3 <math>\rightarrow</math> Constant Pressure</p> $W.D = P_2 V_3 - P_2 V_2 = P_2 (V_3 - V_2) = P_2 (V_1 - V_2)$ $= 5 \times 10^2 \times (0.05 - 0.1)$ $= -25 \text{ KJ}$	02 Marks
	<p>3-1 <math>\rightarrow</math> Constant Volume <math>= W.D = 0</math></p> $W_{net} = W_2 + W_3 + W_1 \Rightarrow 50 - 25 + 0 \Rightarrow 25 \text{ KJ}$	02 Marks
4a.	<p>SFEE</p> $\left[ u_1 + g_1 z_1 + \frac{v_1^2}{2} + g z_1 \right] + Q = \left[ u_2 + g_2 z_2 + \frac{v_2^2}{2} + g z_2 \right] + W$ <p><u>Boiler <math>\Rightarrow</math></u></p> $\Delta V = 0, \Delta \text{Elevation} = 0 \Rightarrow W_{out} = 0$ $Q = \Delta h$ $Q = m \Delta h = m(h_{in} - h_{out})$ <p><u>Nozzle</u></p> $\Delta \text{Elevation} = 0, Q = 0, W = 0$ $h_1 + \frac{v_1^2}{2} = h_2 + \frac{v_2^2}{2}$ <p><u>Centrifugal Pump</u></p> <p>Velocity, Elevation, <math>Q = 0</math>      <math>W = \Delta H = m \Delta h</math></p> <p><math>W = m [h_{in} - h_{out}]</math></p>	

Question Number	Solution	Marks Allocated
	<p><u>Throttling Device</u></p> <p><math>\Delta \text{Velocity} = 0, \Delta \text{Elevation} = 0, Q = 0, W = 0</math></p> <p><math>\Delta H = 0 \Rightarrow h_{\text{in}} = h_{\text{out}} \Rightarrow h_{\text{in}} = h_{\text{out}}</math></p>	$5 \times 2 =$ to Marks
	<p><u>Turbine</u></p> <p><math>\Delta \text{Velocity}, \Delta \text{Elevation}, Q = 0</math></p> <p><math>W = \Delta H = m \Delta h \quad W = m [h_{\text{in}} - h_{\text{out}}]</math></p>	
b.	<p><u>Given</u></p> <p><math>m = 220 \text{ kg/min} \quad Q = -100 \text{ kW/s}</math></p> <p><math>v_1 = 320 \text{ m/s} \quad v_2 = 140 \text{ m/s}</math></p> <p><math>p_1 = 2 \text{ bar} \quad p_2 = 1.2 \text{ bar}</math></p> <p><math>u_1 = 2000 \text{ kJ/kg} \quad u_2 = 1400 \text{ kJ/kg}</math></p> <p><math>\dot{V}_1 = 0.32 \text{ m}^3/\text{kg} \quad \dot{V}_2 = 1.3 \text{ m}^3/\text{kg}</math></p> <p><math display="block">\left[ u_1 + \dot{V}_1 v_1 + \frac{v_1^2}{2} + g z_1 \right] + Q = \left[ u_2 + \dot{V}_2 v_2 + \frac{v_2^2}{2} + g z_2 \right] + W</math></p> <p><math display="block">W = \left[ \left( u_1 - u_2 \right) + \frac{\dot{V}_1 v_1 - \dot{V}_2 v_2}{2 \times 1000} + \frac{v_1^2 - v_2^2}{2 \times 1000} \right] \times \frac{220}{60} - 100</math></p> <p><math display="block">W = \frac{220}{60} \left[ 600 + \frac{6 \times 10^5 \times 0.32 - 1.2 \times 10^5 \times 1.3 + \frac{320^2 - 140^2}{2000}}{2000} \right] - 100</math></p> <p><math display="block">3.67 \left[ 600 + 30 + 41.4 \right] - 100</math></p> <p><math>P = 681.98 \text{ kW} = 0.6 \text{ MW}</math></p>	$02 \text{ Marks}$ $04 \text{ Marks}$ $02 \text{ Marks}$ $02 \text{ Marks}$

Question Number	Solution	Marks Allocated
5a	<p>Equivalence of Kelvin - Planck and Clausius</p> <p>Statements</p>	05 Marks
b.	<p>Equivalence of Clausius and Kelvin Planck Statement</p>	02 Marks
	$\eta = \frac{T_1 - T_2}{T_1} = \frac{W}{Q_1} = \frac{Q_1 - Q_2}{Q_1}$ $\Rightarrow \frac{2100 - Q_2}{2100} = \frac{873 - 313}{873}$ $Q_2 = 752.92 \text{ kJ}$	04 Marks

Question Number	Solution	Marks Allocated
	<p>Then</p> $W_1 = Q_1 - Q_2 = 2100 - 752.9 = 1347.1 \text{ kJ}$ $W_{\text{net}} = W_1 - Q_5$ $Q_5 = W_1 - W_{\text{net}} = 1347.1 - 366 = 987.1 \text{ kJ}$	02 Marks
	<p>In case of refrigeration</p> $W_{\text{in}} = Q_4 - Q_3 = Q_5$ $\varepsilon_R = \frac{T_3}{T_4 - T_3} = \frac{253}{313 - 253} = 4.21$ $Q_3 = \varepsilon_R \times W_{\text{in}} = \varepsilon_R \times Q_5$ $Q_3 = 4.21 \times 987.1 = 4162.21 \text{ kJ}$	02 Marks
b. a.	<p>Entropy is a property and it does not follow the path it depends on the initial and final points. with T-v diagram</p>	04 Marks
b.	<p>Maximum work attainable from a finite Body and a thermal Energy Reservoir</p>  $\Delta S_A = \int_{T_A}^{T_R} C_p \frac{dT}{T} = C_p \ln \frac{T_R}{T_A}$ $\Delta S_{H.E.R.} \neq dS = 0$ $\Delta S_{TER} = \frac{Q_A - W}{T_R}$ $\Delta S_{\text{univ}} = C_p \ln \frac{T_R}{T_A} + \frac{Q_A - W}{T_R}$ <p>Solving <math>W_{\max} = C_p \left[ (T_A - T_R) + T_R \ln \frac{T_R}{T_A} \right]</math></p>	10 Marks

Question Number	Solution	Marks Allocated
c.	<p>Energy lost by temp of Steel = Energy gained by the oil</p> $(m c_s \Delta T)_{\text{steel}} = (m c_o \Delta T)_{\text{oil}}$ $m_s q_s (T_s - T_f) = m_o c_o (T_f - T_o)$ $10 \times 0.5 (900 - T_f) = 100 \times 3.5 (T_f - 303)$ $900 - T_f = 70 T_f - 21210$ $T_f = 311.408 \text{ K}$	02 Marks
	<p>Entropy change in Steel = <math>\Delta S_s = m_s q_s \ln \frac{T_f}{T_s}</math></p> $= 10 \times 0.5 \times \ln \frac{311.408}{900}$ $= -5.301 \text{ J/K}$	01 More
	<p>Entropy change in oil = <math>\Delta S_o = m_o q_o \ln \frac{T_f}{T_o}</math></p> $= 100 \times 3.5 \times \ln \frac{311.408}{303}$ $= 4.16 \text{ J/K}$	01 More
	$(\Delta S)_{\text{universe}} = \Delta S_{\text{steel}} + \Delta S_{\text{oil}}$ $= -1.1425 \text{ J/K}$	02 More
7. a.	definition / concept of available & unavailable energy	4 Marks
b.	Maxwell relations	
	$\left( \frac{\partial T}{\partial V} \right)_S = - \left( \frac{\partial P}{\partial S} \right)_V = \frac{\partial^2 U}{\partial S \partial V}$	
	$\left( \frac{\partial T}{\partial P} \right)_S = \left( \frac{\partial V}{\partial S} \right) = \frac{\partial^2 H}{\partial S \partial P}$	

Question Number	Solution	Marks Allocated
	$\left(\frac{\partial S}{\partial V}\right)_T = \left(\frac{\partial P}{\partial V}\right)_T = -\frac{\partial^2 f}{\partial T \partial V}$ $-\left(\frac{\partial S}{\partial P}\right)_T = \left(\frac{\partial V}{\partial T}\right)_P = \frac{\partial^2 G}{\partial T \partial P}$	
c.	$V = 0.04 \text{ m}^3$ $t_3 = 250^\circ\text{C}$ $m_f = 9 \text{ kg}$ From steam table @ $250^\circ\text{C}$ $P_s = 39.73 \text{ bar}$	0.6 Marks
	$v_f = 0.0012512 \text{ m}^3/\text{kg}$ $v_g = 0.05013 \text{ m}^3/\text{kg}$ $h_f = 1085.36 \text{ J/g}$ $h_{fg} = 2716.25 \text{ J/g}$ $s_f = 2.7927 \text{ kJ/kgK}$ $s_{fg} = 3.2862 \text{ kJ/kgK}$	0.1 Marks
	$v_g = \text{volume of dry steam} = V - v_f$ $= V - m_f (v_f)$ $= 0.04 - 9 \times 0.0012512$ $= 0.02874 \text{ m}^3$	0.1 Marks
	$\text{Mass of dry steam} = \frac{0.02874}{0.05013} = 0.5733 \text{ kg}$	
	$\text{Mass of steam} = m_g + m_f = 0.5733 + 9 = 9.5733$	0.1 Marks
	$\text{Specific Volume} = V = v_f + x v_{fg}$ $x = \frac{m_g}{m_g + m_f} = \frac{0.5733}{0.5733 + 9} = 0.06$	

Question Number	Solution	Marks Allocated
	$V = 0.0012512 + 0.01(0.5013 - 0.0012512)$ $= 0.0041839 \text{ m}^3/\text{kg}$	01 Marks
	Specific enthalpy = $h_f + xh_{fg} = 1188.332 \text{ kJ/kg}$	02 Marks
	Specific entropy = $s_f + x s_{fg} = 2.9895 \text{ kJ/kg K}$	02 Marks
	Specific Internal energy $u = h - PV$ $= 1171.709 \text{ kJ/kg}$	01 Marks
8a.	Working of combined Separating and Throttling Calorimeter Diagram Explanation & Equation	5 Marks
	$\lambda_1 = \frac{M}{m+M}$ $\lambda_2 = \frac{h_{up. C} - h_f \cdot B}{h_f \cdot B}$ $x = \frac{M \cdot \lambda_2}{m+M}$	05 Marks
b.	$P = 10 \text{ bar}$ $x = 0.15$ $W.D. = P(V_2 - V_1)$ using steam tables	

Question Number	Solution	Marks Allocated
	<p>finding change in enthalpy Heat transferred change in entropy</p>	10 Marks
a.	<p>Vanderwaal's equation / constant in terms of critical properties</p> $\left(1 + \frac{a}{v^2}\right) (v - b) = RT$ $\frac{V_c}{b} = 3 \quad T_c = \frac{8a}{27Rb} \quad a = 3V_c^2 P_c$	08 Marks
b.	Definition of Generalized compressibility chart	4 Marks
c.	<p><math>v = 1.5 \text{ m}^3</math> <math>m = 5 \text{ kg}</math> <math>T = 300 \text{ K}</math></p> <p>Ideal gas</p> $P_v = mRT$ $P = \frac{mRT}{v} = \frac{5 \times \frac{8314}{44}}{1.5} \times 300 = 1.889 \text{ bar}$ <p>Vanderwaal's eqn</p> $P = \frac{RT}{v-b} - \frac{a}{v^2}$ $\Rightarrow \frac{8314 \times 300}{6.82 - 0.0427} - \frac{364.3 \times 10^3}{(6.82)^2}$ $= 368022.6 - 7832.3$ $= 3.6 \text{ bar}$	

10.  
a Dalton's + Amagat's law Definition

03 Marks

b. Expression for I.F and Enthalpy

04 Marks

c. 1 kg - CO<sub>2</sub>

1.5 kg - N<sub>2</sub>

P = 3.5 bar T = 27°C

i) Mole fraction

$$n = \frac{m}{M} \quad n_{CO_2} = \frac{1}{44} = 0.022$$

$$n_{N_2} = \frac{1.5}{28} = 0.053$$

$$X_{CO_2} = \frac{0.022}{0.022 + 0.053} = 0.2933$$

$$X_{N_2} = \frac{0.053}{0.022 + 0.053} = 0.7066$$

ii) Partial Pressures

$$P_{CO_2} = n_{CO_2} R T$$

$$P_{CO_2} = \frac{n_{CO_2} R T}{V} = \frac{0.022 \times 8.314 \times 10^3 \times 300}{V}$$

$$V = \frac{mRT}{P} = \frac{2.5 \times R \times 300}{M \times 3.5 \times 10^5}$$

$$M = \frac{n_{CO_2} N_{CO_2} + n_{N_2} N_{N_2}}{n_{CO_2} + n_{N_2}}$$

$$= \frac{2.5 \times 8.314 \times 300}{32.69 \times 3.5 \times 10^5} = \frac{0.022 \times 44 + 0.053 \times 28}{0.022 + 0.053}$$

$$= \frac{2.5 \times 0.254 \times 10^3 \times 300}{32.69 \times 3.5 \times 10^5} = \boxed{32.69 = M}$$

$$\therefore 0.5442 m^3$$

$$P_{CO_2} = 1.0083 \text{ bar} \quad P_{N_2} = 2.491 \text{ bar}$$

"APPROVED"  
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10 Marks